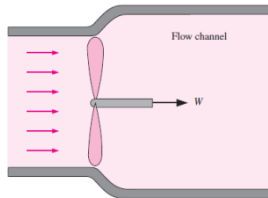


Question 2

Windmills slow down the air and cause it to fill a larger channel as it passes through the blades. Consider a circular windmill with a 7-m diameter rotor in a 10 m/s wind on a day with an atmospheric pressure of 100 kPa and a temperature of 20 Celsius. The wind speed behind the windmill is measured at 9 m/s. Determine the diameter of the channel downstream from the rotor and the power produced by this windmill, presuming that the air is incompressible.



Answer 2

The flow of air through a flow channel is considered. The diameter of the wind channel downstream from the rotor and the power produced by the windmill are to be determined.

**Analysis** The specific volume of the air is

$$\nu = \frac{RT}{P} = \frac{(0.287 \text{ kPa} \cdot \text{m}^3/\text{kg} \cdot \text{K})(293 \text{ K})}{100 \text{ kPa}} = 0.8409 \text{ m}^3/\text{kg}$$

The diameter of the wind channel downstream from the rotor is

$$A_1V_1 = A_2V_2 \longrightarrow (\pi D_1^2 / 4)V_1 = (\pi D_2^2 / 4)V_2$$

$$\longrightarrow D_2 = D_1 \sqrt{\frac{V_1}{V_2}} = (7 \text{ m}) \sqrt{\frac{10 \text{ m/s}}{9 \text{ m/s}}} = \mathbf{7.38 \text{ m}}$$

The mass flow rate through the wind mill is

$$\dot{m} = \frac{A_1V_1}{\nu} = \frac{\pi(7 \text{ m})^2(10 \text{ m/s})}{4(0.8409 \text{ m}^3/\text{kg})} = 457.7 \text{ kg/s}$$

The power produced is then

$$\dot{W} = \dot{m} \frac{V_1^2 - V_2^2}{2} = (457.7 \text{ kg/s}) \frac{(10 \text{ m/s})^2 - (9 \text{ m/s})^2}{2} \left( \frac{1 \text{ kJ/kg}}{1000 \text{ m}^2/\text{s}^2} \right) = \mathbf{4.35 \text{ kW}}$$

Question 3 :

A 0.2 m<sup>3</sup> fully insulated rigid container is divided into two equal volumes by ony a thin membrane. Initially, one of these chambers is filled with air at a pressure of 700 kPa and 37 °C while the other chamber is evacuated.

$$C_p = 1.005 \text{ kJ/kg.K} \quad C_v = 0.721 \text{ kJ/kg.K}$$

- a) Determine the change in internal energy of the air when the membrane is ruptured.
- b) Determine the final air pressure in the container

////////////////////////////////////

Answer 3

- a) The total internal energy does not change. Therefore, the temperature does not change
- b) Given that the ideal gas law applies, the pressure is halved and becomes 350 kPa

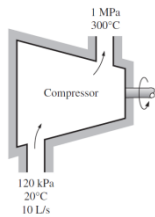
Question 4:

An adiabatic air compressor compresses 10 liter/s of air as 120 kPa and 20<sup>o</sup> C to 1000 kPa and 300<sup>o</sup> C.

At room temperature:  $C_p = 1.005 \text{ kJ/kg}\cdot\text{K}$        $C_v = 0.721 \text{ kJ/kg}\cdot\text{K}$ . At 300<sup>o</sup> C :  $C_p = 1.031 \text{ kJ/kg}\cdot\text{K}$   
 $C_v = 0.753 \text{ kJ/kg}\cdot\text{K}$ ;  $R_{\text{air}} = 0.287 \text{ kPa}\cdot\text{m}^3/\text{kg}\cdot\text{K}$

Determine

- The amount of work required by the compressor in kJ/kg and
- The power required to drive the air compressor in kW



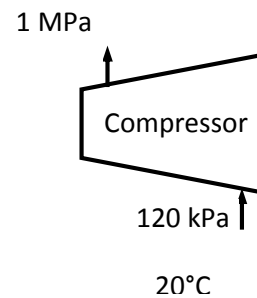
**Analysis (a)** There is only one inlet and one exit, and thus  $\dot{m}_1 = \dot{m}_2 = \dot{m}$ . We take the compressor as the system, which is a control volume since mass crosses the boundary. The energy balance for this steady-flow system can be expressed in the rate form as

$$\underbrace{\dot{E}_{\text{in}} - \dot{E}_{\text{out}}}_{\text{Rate of net energy transfer by heat, work, and mass}} = \underbrace{\dot{\Delta E}_{\text{system}}}_{\substack{\approx 0 \text{ (steady)} \\ \text{Rate of change in internal, kinetic, potential, etc. energies}}} = 0$$

$$\dot{E}_{\text{in}} = \dot{E}_{\text{out}}$$

$$\dot{W}_{\text{in}} + \dot{m}h_1 = \dot{m}h_2 \quad (\text{since } \Delta ke \cong \Delta pe \cong 0)$$

$$\dot{W}_{\text{in}} = \dot{m}(h_2 - h_1) = \dot{m}c_p(T_2 - T_1)$$



Thus,

$$w_{\text{in}} = c_p(T_2 - T_1) = (1.018 \text{ kJ/kg}\cdot\text{K})(300 - 20)\text{K} = \mathbf{285.0 \text{ kJ/kg}}$$

(b) The specific volume of air at the inlet and the mass flow rate are

$$v_1 = \frac{RT_1}{P_1} = \frac{(0.287 \text{ kPa}\cdot\text{m}^3/\text{kg}\cdot\text{K})(20 + 273 \text{ K})}{120 \text{ kPa}} = 0.7008 \text{ m}^3/\text{kg}$$

$$\dot{m} = \frac{\dot{V}_1}{v_1} = \frac{0.010 \text{ m}^3/\text{s}}{0.7008 \text{ m}^3/\text{kg}} = 0.01427 \text{ kg/s}$$

Then the power input is determined from the energy balance equation to be

$$\dot{W}_{\text{in}} = \dot{m}c_p(T_2 - T_1) = (0.01427 \text{ kg/s})(1.018 \text{ kJ/kg}\cdot\text{K})(300 - 20)\text{K} = \mathbf{4.068 \text{ kW}}$$

Question 5:

A geothermal plant uses geothermal water extracted at 160° C at a rate of 440 kg/s as the heat source. The actual rate of heat rejection from this plant is 22 MW and produces 22 MW of net power. If the environmental temperature is 25° C, determine

- a) The actual thermal efficiency
- b) The maximum possible thermal efficiency

The water is to be regarded as a saturated liquid at all times

////////////////////////////////////

**6-88** A geothermal power plant uses geothermal liquid water at 160°C at a specified rate as the heat source. The actual and maximum possible thermal efficiencies and the rate of heat rejected from this power plant are to be determined.

**Assumptions** **1** The power plant operates steadily. **2** The kinetic and potential energy changes are zero. **3** Steam properties are used for geothermal water.

**Properties** Using saturated liquid properties, the source and the sink state enthalpies of geothermal water are (Table A-4)

$$\left. \begin{array}{l} T_{\text{source}} = 160^{\circ}\text{C} \\ x_{\text{source}} = 0 \end{array} \right\} h_{\text{source}} = 675.47 \text{ kJ/kg}$$

$$\left. \begin{array}{l} T_{\text{sink}} = 25^{\circ}\text{C} \\ x_{\text{sink}} = 0 \end{array} \right\} h_{\text{sink}} = 104.83 \text{ kJ/kg}$$

**Analysis** (a) The rate of heat input to the plant may be taken as the enthalpy difference between the source and the sink for the power plant

$$\dot{Q}_{\text{in}} = \dot{m}_{\text{geo}}(h_{\text{source}} - h_{\text{sink}}) = (440 \text{ kg/s})(675.47 - 104.83) \text{ kJ/kg} = 251,083 \text{ kW}$$

The actual thermal efficiency is

$$\eta_{\text{th}} = \frac{\dot{W}_{\text{net,out}}}{\dot{Q}_{\text{in}}} = \frac{22 \text{ MW}}{251.083 \text{ MW}} = \mathbf{0.0876 = 8.8\%}$$

(b) The maximum thermal efficiency is the thermal efficiency of a reversible heat engine operating between the source and sink temperatures

$$\eta_{\text{th,max}} = 1 - \frac{T_L}{T_H} = 1 - \frac{(25 + 273) \text{ K}}{(160 + 273) \text{ K}} = \mathbf{0.312 = 31.2\%}$$

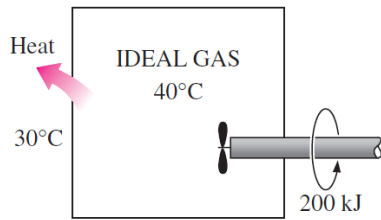
(c) Finally, the rate of heat rejection is

$$\dot{Q}_{\text{out}} = \dot{Q}_{\text{in}} - \dot{W}_{\text{net,out}} = 251.1 - 22 = \mathbf{229.1 \text{ MW}}$$

Question 6:

A rigid tank contains an ideal gas at 40° C that is being stirred by a paddle wheel. The paddle wheel does 200 kJ of work on the ideal gas. It is observed that the temperature of the ideal gas remains constant during the stirring as a result of the heat transfer between the system and the surroundings which is at 30° C.

Determine the entropy change of the ideal gas



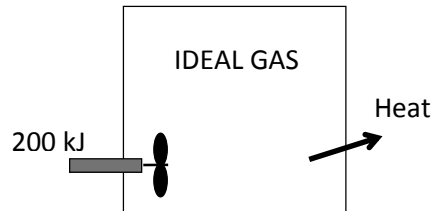
Answer 6

**7-23** A rigid tank contains an ideal gas that is being stirred by a paddle wheel. The temperature of the gas remains constant as a result of heat transfer out. The entropy change of the gas is to be determined.

**Assumptions** The gas in the tank is given to be an ideal gas.

**Analysis** The temperature and the specific volume of the gas remain constant during this process. Therefore, the initial and the final states of the gas are the same. Then  $s_2 = s_1$  since entropy is a property. Therefore,

$$\Delta S_{\text{sys}} = 0$$



Question 7 :

Air is being used as the working fluid in a simple ideal Brayton cycle that has a pressure ratio of 12, a compressor inlet temperature of 300 K and a turbine inlet temperature of 1000K.

- a) Determine the required mass flow rate of air for a net power output of 70 MW, assuming that both the compressor and the turbine have an isentropic efficiency of 100 %
- b) Determine the required mass flow rate of air for a net power output of 70 MW, assuming that both the compressor and the turbine have an isentropic efficiency of 85 %

////////////////////////////////////

Answer 7:

**9-98** A gas turbine power plant that operates on the simple Brayton cycle with air as the working fluid has a specified pressure ratio. The required mass flow rate of air is to be determined for two cases.

**Assumptions** 1 Steady operating conditions exist. 2 The air-standard assumptions are applicable. 3 Kinetic and potential energy changes are negligible. 4 Air is an ideal gas with constant specific heats.

**Properties** The properties of air at room temperature are  $c_p = 1.005 \text{ kJ/kg}\cdot\text{K}$  and  $k = 1.4$  (Table A-2).

**Analysis** (a) Using the isentropic relations,

$$T_{2s} = T_1 \left( \frac{P_2}{P_1} \right)^{(k-1)/k} = (300 \text{ K})(12)^{0.4/1.4} = 610.2 \text{ K}$$

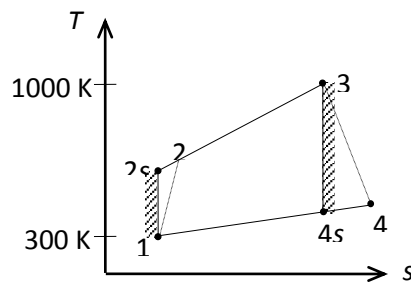
$$T_{4s} = T_3 \left( \frac{P_4}{P_3} \right)^{(k-1)/k} = (1000 \text{ K}) \left( \frac{1}{12} \right)^{0.4/1.4} = 491.7 \text{ K}$$

$$w_{s,C,in} = h_{2s} - h_1 = c_p (T_{2s} - T_1) = (1.005 \text{ kJ/kg}\cdot\text{K})(610.2 - 300)\text{K} = 311.75 \text{ kJ/kg}$$

$$w_{s,T,out} = h_3 - h_{4s} = c_p (T_3 - T_{4s}) = (1.005 \text{ kJ/kg}\cdot\text{K})(1000 - 491.7)\text{K} = 510.84 \text{ kJ/kg}$$

$$w_{s,net,out} = w_{s,T,out} - w_{s,C,in} = 510.84 - 311.75 = 199.1 \text{ kJ/kg}$$

$$\dot{m}_s = \frac{\dot{W}_{net,out}}{w_{s,net,out}} = \frac{70,000 \text{ kJ/s}}{199.1 \text{ kJ/kg}} = \mathbf{352 \text{ kg/s}}$$



(b) The net work output is determined to be

$$w_{a,net,out} = w_{a,T,out} - w_{a,C,in} = \eta_T w_{s,T,out} - w_{s,C,in} / \eta_C$$

$$= (0.85)(510.84) - 311.75 / 0.85 = 67.5 \text{ kJ/kg}$$

$$\dot{m}_a = \frac{\dot{W}_{net,out}}{w_{a,net,out}} = \frac{70,000 \text{ kJ/s}}{67.5 \text{ kJ/kg}} = \mathbf{1037 \text{ kg/s}}$$